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REMARKS

Claims 12-19 are in the case.

Claims 12-19 have been amended to more particularly point out and distinctly claim that which Applicants regard as their invention and comply with the Examiner's suggestions.

35 U.S.C. §112

Claims 12-19 stand rejected under 35 U.S.C. §112, second paragraph, as indefinite. Claims 12-19 have been amended to more particularly point out and distinctly claim that which Applicants regard as their invention and to comply with the Examiner's suggestions. It is believed that the amendments to the claims have corrected the indefiniteness, and the rejection of Claims 12-19 under 35 U.S.C. §112, second paragraph, is respectfully requested to be withdrawn.

35 U.S.C. §102

Claims 12-16 stand rejected under 35 U.S.C. §102(b) as anticipated by Faylor et al. U.S. Patent No. 3,870,033 (hereinafter "Faylor").

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Faylor discloses a deionized pretreated supply water and passing a part of the stored water through a pure water recirculation loop.

Applicant's Claims 12-16 require treating a wastewater feed containing metal ions in solution, which is nowhere taught or suggested in Faylor. On the contrary, Faylor discloses the ability to remove ions with an ion-exchange resin with a pure water feed that has no suspended solids. Faylor nowhere mentions or uses the presence of high levels of solids. The difference is important because Applicants' invention as claimed provides for the passing of the solids-containing waste slurry without appreciable retention in the column and the removal of peroxide and copper occurring with the passage of solids (50 to > 2000 mg/l). High solids feeds are passed through packed columns without the solids impacting the performance of that column.

For the foregoing reasons, the rejection of Claims 12-16 under 35 U.S.C. §102(b) as anticipated by Faylor et al. U.S. Patent No. 3,870,033 is based on an insufficient reference and is respectfully requested to be withdrawn.

35 U.S.C. §103

Claims 17-19 stand rejected under 35 U.S.C. §103(a) as unpatentable over Faylor et al. U.S. Patent No. 3,870,033 (here

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inafter "Faylor") in view of Katzakian U.S. Patent No. 3,928,192 (hereinafter "Katzakian").

Applicants' invention as claimed provides a novel process and apparatus for the removal of copper ions including passing a wastewater solution containing copper ions first through a carbon adsorption column, preferably without prior micro-filtration or ultra-filtration removal of silica, alumina slurry solids, to remove catalytically the hydrogen peroxide (H_2O_2) and then contacting the wastewater solution containing copper ions to attach the copper, preferably with a chelating ion exchange resin of iminodiacetic functional group.

Faylor discloses a deionized pretreated supply water and passing a part of the stored water through a pure water recirculation loop. Applicants' Claims require treating a wastewater feed containing metal ions in solution, which is nowhere taught or suggested in Faylor. On the contrary, Faylor discloses the ability to remove ions with an ion-exchange resin with a pure water feed that has no suspended solids. Faylor nowhere mentions or uses the presence of high levels of solids. The difference is important because Applicants' invention as claimed provides for the passing of the solids-containing waste slurry without appreciable retention in the column and the removal of peroxide and copper occurring with the passage of solids (50 to > 2000 mg/l).

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High solids feeds are passed through packed columns without the solids impacting the performance of that column.

Katzakian discloses water demineralizing using separate beds of weakly acidic cation exchange resin, weakly basic anion exchange resin, and a third column of weakly acidic cation exchange resin. A saline feed is passed through the system.

There is no motivation to combine the Faylor and Katzakian references. Even assuming, but not granting or admitting that one would have combined the Faylor and Katzakian references, one would not have come up with Applicants' invention as claimed of a novel process and apparatus for the removal of copper ions by passing a wastewater solution containing copper ions first through a carbon adsorption column, preferably without prior micro-filtration or ultra-filtration removal of silica, alumina slurry solids, to remove catalytically the hydrogen peroxide (H_2O_2) and then contacting the wastewater solution containing copper ions to attach the copper, preferably with a chelating ion exchange resin of iminodiacetic functional group, except on the basis of reconstructive hindsight after having had the benefit of Applicants' full disclosure as set forth in the detailed description of Applicants' Specification.

Applicants' invention as claimed passes the solids-containing waste slurry without appreciable retention in the column and

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removes peroxide and copper occurring with the passage of solids (50 to > 2000 mg/l). A high solids feed is passed through packed columns without the solids impacting the performance of that column. This is not intuitively obvious and has not been for many years. Further evidence of the non-obviousness of Applicants' invention as claimed is observed in the feed specification published by the ion exchange resin manufacturer, which specifies a critical feed quality limitation as having a turbidity of <5 NTU's or in some cases <1 NTU. A chemical mechanical polishing CMP wastewater slurry is opaque, not transmitting to light, and infinitely outside the range of these feed specifications. Subsequent work in the field has been run with feeds having suspended solids in excess of 20% by weight (i.e. 200,000 mg/l).

Faylor discloses the ability to remove ions with ion-exchange resin with a pure water feed that has no suspended solids. This is obvious and the presence of high levels of solids is not addressed.

Faylor is significantly different from Applicants' invention as claimed. Faylor uses a variety of filtration devices, i.e., diatomaceous filters and/or pretreatment steps, i.e., alum/soda coagulation/flocculation followed by sand filtration to remove solids prior to carbon filtration. Applicants' invention as claimed differs significantly in that Applicants' invention does

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not remove suspended solids ahead of the carbon filter/ion exchange process for removing heavy metals. Applicants' invention as claimed has the distinct advantage in high solids loading applications such as this, of letting the solids which are largely non-regulated solids pass through the oxidant removal steps and through the ion exchange step. The copper, a commonly regulated metal, is removed in the ion exchange system, where it can be regenerated to form a concentrated copper solution that is recoverable by electrolytic recovery process or by specialized precipitation processes which precipitate the copper in a form suitable for resale. The copper-free solids then can be discharged to a sewer, if the suspended solids levels of this stream when combined with the remainder of the plant's effluent are below regulatory limits.

Alternately, the copper-free solids can be removed by coagulation and settling, direct filtration, and disposed of according to appropriate regulations.

Applicants' invention as claimed differs from prior art in that Applicants' invention provides a proper control of system chemistry to feed water with up to 2000+ mg/l of suspended solids material through a carbon column without plugging the column or removing any appreciable amounts of suspended solids. This is counter-intuitive to what anyone versed in the art of water

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treatment would expect. Additionally, removing the peroxide is necessary to obtain a reasonable life for the ion exchange resin. Peroxide in the presence of heavy metals, such as copper, can produce hydroxyl radicals (Fenton's Reageant) which degrade ion exchange resin polymers.

Applicants' invention as claimed provides a novel process and apparatus for the removal of copper ions from a byproduct polishing slurry wastewater solution containing copper from the chemical mechanical polishing (CMP) of integrated circuits of semiconductor microelectronic chips. The chemical mechanical polishing (CMP) planarization process introduces copper into the process water, and governmental regulations for the discharge of wastewater from the chemical mechanical polishing (CMP) planarization process are as stringent as the wastewater from an electroplating process, even though CMP planarization is not an electroplating process. The copper ions in solution in the wastewater must be removed from the byproduct polishing slurry for acceptable wastewater disposal. The chemical mechanical polishing planarization of the microchip produces a byproduct "grinding" (polishing) slurry wastewater which contains copper ions at a level of about 1-100 mg/l. The byproduct polishing slurry wastewater from the planarization of the microchip also

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contains solids sized at about 0.01-1.0 μm at a level of about 500-2000 mg/l (500-2000 ppm). An oxidizer of hydrogen peroxide (H_2O_2) typically is used to help dissolve the copper from the microchip. Accordingly, hydrogen peroxide (H_2O_2) at a level of about 300 ppm and higher also is present in the byproduct polishing slurry wastewater. A chelating agent such as citric acid or ammonia also can be present in the byproduct polishing slurry to facilitate keeping the copper in solution. If hydrogen peroxide (H_2O_2) is present, the ion exchange resin will be oxidized, and the resin structure is broken down. Accordingly, hydrogen peroxide can not be present in an ion exchange unit operation because the ion exchange resin is incompatible with hydrogen.^{oxidizing agents}

Ion exchange can be used to attach copper ions, but would not be likely to work on a byproduct polishing slurry because of the quantities of solids coming in with the byproduct polishing slurry in the form of a silica, alumina slurry. Conventional pretreatment practice for granular activated carbon beds principally requires the removal of contaminants such as excess amounts of suspended solids. Suspended solids, including bacteria, in amounts exceeding about 50 mg/l (50 ppm), and commonly in amounts exceeding about 5 mg/l (5 ppm) are required to be removed prior to operating the carbon bed. Ion exchange resin suppliers and

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equipment manufacturers strongly advise that particle controls ahead of, i.e., upstream from, ion exchange bed systems are an essential aspect of an effective pretreatment system. Particles of suspended solids bind up the ion exchange resin beds. The resin acts as a filter to retain the particles. The suspended solids accumulate and cause an increase in pressure drop across the resin bed. When this increased pressure drop occurs, the water is forced to take the path of least resistance and circumvents or flows around the resin bed. This resin circumvention is called channeling. When the process water flows down the sides of the column, a large portion of the resin is bypassed, limiting the contact between the resin and the process water, resulting in high contaminant leakage and poor bed capacity. Under extreme conditions, internal distributors and collectors can break due to the high pressure drop. An ion exchange bed that is loaded with solids is difficult to regenerate. The regenerant solution takes the path of least resistance and channels down the sides of the column resulting in incomplete regeneration of the resin.

According to Rohm and Haas, the feed must be relatively free from suspended and colloidal material. The suspended and colloidal matter will form a mat at the surface of the bed. Pressure drop increases, channeling is encountered, and portions of the bed are

by-passed. The suspended and colloidal matter also coat the beads and granules of the ion exchange resin, reducing the rate of diffusion of ions in and out of the exchanger resin. It is therefore important that all feeds be clarified as much as possible to remove the last traces of suspended or colloidal matter. Coagulation, sedimentation, and filtration are the normal clarifying methods. The byproduct polishing slurry wastewater containing copper ions from the CMP of semiconductor micro-electronic chips containing copper can be passed through a micro-filter to remove the solids in the form of the silica, alumina slurry. The permeate from the microfilter containing permeate copper ions then can be contacted with the ion exchange resin to attach the copper. Further according to Rohm and Haas, pretreatment of the feed also should remove or neutralize traces of soluble constituents that may degrade or foul the exchanger, e.g., traces of oxygen, ozone, chlorine, and other oxidants. Wastewaters from non-copper CMP processes are generally discharged to the semiconductor fabrication facility end-of-pipe where the wastewater is neutralized prior to discharge. With the advent of copper technology, these slurry wastewaters will contain copper. Copper present in the fabrication facility outfall poses problems. Some fabrication facilities must control

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the amount of suspended solids in the out fall. Accumulation in the receiving POTW's (Publicly Owned Treatment Works) sludges result in increased cost for municipal sludge disposal and environmental concerns to eliminate copper in the municipal sludge. Bio-toxicity problems in the municipal biological systems are caused by mass loading of copper. Environmental discharge limits for copper result in non-compliance at the fabrication facility.

Applicants' process and apparatus as claimed overcome all of these problems and remove the copper from the waste slurries near the point of generation and permit a copper-free waste to pass to discharge and neutralization. Applicants' process and apparatus as claimed overcome all of these problems and remove copper ions from solution for acceptable wastewater disposal of byproduct polishing slurries containing high amounts of suspended solids and remove the copper ions from solution containing high amounts of suspended solids efficiently and economically.

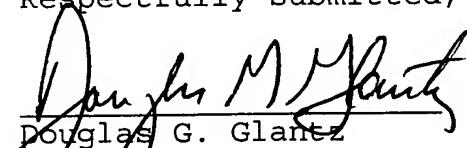
For the foregoing reasons, the rejection of Claims 17-19 under 35 U.S.C. §103(a) as unpatentable over Faylor et al. U.S. Patent No. 3,870,033 in view of Katzakian U.S. Patent No. 3,928,192 is based on an improper combination of insufficient references and is respectfully requested to be withdrawn.

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Attached hereto is a marked-up version of the changes made to the Abstract by the current Amendment. The attached pages are captioned "VERSION WITH MARKINGS TO SHOW CHANGES MADE."

Reconsideration of this application is requested.

Respectfully submitted,



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VERSION WITH MARKINGS TO SHOW CHANGES MADE

12. Apparatus for removing metal ions from wastewater, comprising:

(a) a carbon bed for receiving a wastewater feed containing metal ions in solution, wherein said wastewater feed contains solids sized in the range of about 0.01-1.0 μm in an amount higher than about 50 mg/l; and

(b) an ion exchange unit [operation] for receiving a carbon bed product stream from said carbon bed and for removing said metal ions from solution.

13. Apparatus for removing metal ions from wastewater as set forth in Claim 12, wherein said wastewater feed contains solids in an amount higher than about 100 mg/l.

14. Apparatus for removing metal ions from wastewater as set forth in Claim 12, wherein said wastewater feed contains hydrogen peroxide and said carbon bed product stream has concentration levels of hydrogen peroxide less than about 0.1 mg/l.

15. Apparatus for removing metal ions from wastewater as set forth in Claim 14, wherein wastewater feed comprises a byproduct

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polishing slurry and said metal ions comprise copper ions in said byproduct polishing slurry.

16. Apparatus for removing metal ions from wastewater as set forth in Claim 15, wherein said wastewater feed comprises a byproduct polishing slurry from the chemical mechanical polishing [(CMP)] of integrated circuits and said metal ions comprise copper ions at a level in the range of about 1-100 mg/l.

17. Apparatus for removing metal ions from wastewater as set forth in Claim 15, wherein said ion exchange unit [operation] comprises organic chemical means for contacting said carbon bed product stream metal ions with a resin having a macroporous iminodiacetic functional group to attach said copper ions.

18. Apparatus for removing metal ions from wastewater as set forth in Claim 15, wherein said ion exchange unit [operation] comprises organic chemical means for contacting said carbon bed product stream metal ions with cross-linked polystyrene resin to attach said copper ions.

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19. Apparatus for removing metal ions from wastewater as set forth in Claim 18, wherein said ion exchange unit [operation] comprises inorganic chemical means for contacting said carbon bed product stream metal ions with cross-linked polystyrene resin having a bead size in the range of about 0.4 to 1.23 mm with a tight uniformity coefficient of about 1.7 to attach said copper ions.